The University of Adelaide

School of Chemical Engineering

Cooperative Research Centre for Clean Power from Lignite

Physical Modelling of Mixing Between Rectangular Jets Present in Tangentially Fired Brown Coal Boilers

Ph.D. Thesis

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..... A tutti coloro che hanno lasciato la loro terra per permettere una vita migliore per i propri figli...... 'I am an old man now, and when I die and go to heaven there are two matters on which I hope enlightenment. One is quantum electrodynamics and the other is turbulence in fluids. About the former I am rather optimistic'.

Sir Horace Lamb, 1932.

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A Mamma e Papa';

Tutto cio' la dedico a voi, gli sacfrici che avete fatto, lasciando la vostra terra per permettermi di asprirare ad una vita migliore, sacrifici che soltano il genitore emigrato possa capire.

Statement of originality

The Material in this thesis is original and has not been submitted or accepted for the award of degree or diploma at any other university and to the best of my knowledge and belief, the thesis contains no material previously published or written by another person except where due reference is made in the text of the thesis.

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Executive Summary

Large scale power generation commences with the combustion of coal or other fuel, which in turn converts high pressure water into steam which then drives a turbine thus generating electricity. Burning high moisture coal, such as lignite, for power generation implies that a significant amount of energy is wasted in vaporising the moisture, which could otherwise be used in the steam raising process. This implies that more moist coal would be required to drive the same process than if the coal was drier, thus increasing the amount of combustion products such as greenhouses gases. Introducing a dried coal in an existing boiler will significantly change the heat flux profiles, which could result in boiler damage or excessive fouling. Flame temperature is influenced by the supply of reactants; in most cases the limiting reactant will be oxygen. The supply of oxygen (through air) to a pneumatically transported coal stream and subsequent reaction is controlled by the localised fluid mechanics or 'mixing'. This research aims to provide an understanding of the mixing process between the pneumatically transported coal and air in brown coal fired boilers by modelling the individual jets. The effects of the change in velocity ratio for the air (secondary) jets and fuel (primary) jets of rectangular burners typical of those found in brown coal fired boilers has been studied experimentally and is reported in this thesis. In particular, scientific analysis was used to investigate the physical mechanisms which control fuel-air mixing, and to quantify the concentration of primary and secondary fluid. The concentration data was used in a regression model in conjunction with a reactive combustion model, developed from a 1:30 scale cold model of the Yallourn W' stage 2 boiler, in order that overall boiler performance can be assessed. This overall study is fundamental as a result of the questions raised concerning the future of brown coal in modern society.

A qualitative flow visualisation study of the unconfined 1:30 scaled primary, and two adjacent rectangular jets, was conducted using single colour planar laser induced fluorescence. The characteristics of the jet flow were examined by imaging individually seeded primary and secondary jets and were visualised through four different planes longitudinally, on the axes of each jet. In addition, a transverse qualitative and quantitative study on the rectangular jets was also conducted for the individually seeded jets, and was visualised through planes of flow perpendicular to the direction flow, specifically at axial stations of x/D = 0.1, 0.2, 0.5, 1, 2, 4, 6 and 8. The flow characteristics were also examined under different co-flow conditions, particularly secondary to primary jet velocity ratios (λ) of 0, 0.55, 1.4, 2.8, 3.6 and ∞ . This quantitative data yields the basis for a 3D regression model to predict fuel-air mixing in actual

boilers. A semi-quantitative investigation into some geometrical modifications on the rectangular jets was also conducted at velocity ratios of λ =0, 0.55 and 1.4. The rectangular nozzles were fitted with base plates orientated at 90 degrees and 60 degrees to the direction of flow.

The longitudinal flow visualisation study highlighted the effect of velocity ratio on the flow field of the primary and secondary jets. In particular it showed that the main structures of the primary and secondary jets are sensitive to the co-flowing conditions. The primary jet also experienced the formation of coherent structures close to the bluff body re-circulation region for λ >2.8. The quantitative transverse analysis of the rectangular jets showed that the primary jet and secondary jets close to the nozzle exit plane distorted with a change in co-flowing conditions. The primary jet experienced distortion for λ >1.4, and the secondary jets experienced distortion for λ <1.4. A plausible mechanism for this "distortion" can be explained by different co-flowing conditions altering the velocity gradients of the jet, thus changing the denomination of the counter rotating vortices present in the corners of rectangular jets, allowing them to alter jet shape.

The transverse quantitative analysis of the rectangular jets allowed for graphical representation of the normalised concentration of the primary and secondary jets in the radial direction and the centreline mixture fraction decay. The analysis of the latter showed that the primary jet, under all co-flow conditions, reached self-similarity at approximately x/D = 4, whereas the secondary jets did so at x/D = 2. The primary jets observed greater rates of centreline dilution at high velocity ratios, whereas the secondary jets did so at $\lambda=0.55$. The quantification of the centreline concentration decay obeyed the inverse rate law for all co-flowing conditions. The first order decay constant K_1 , was found to be heavily dependent on velocity ratio.

The planar transverse quantitative data of the primary and secondary jets was used with the method of weighted squares to develop a regression model that would three-dimensionally reproduce the scalar mixing field as a function of velocity ratio. The regression model reproduces scalar quantities for λ =0 and λ =0.55 to 3.6 for the primary jet and λ =0.55 to 3.6 and ∞ for the secondary jet, and is capable of predicting primary and secondary bulk fluid concentrations within 30 to 40 % of the measured values. A sensitivity analysis on the regression model revealed that it is highly responsive to the momentum-controlling region between the jets with a change in velocity ratio.

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Figure D. 22:	Schematic diagram of the entrainment of free stream fluid into the primary jet
	through plane C
Figure D. 23:	Comparison of the secondary decay constant K_2 versus velocity ratio for the
	Primary jet under free conditions and with a base plate orientated at 60 degrees to
	the flow through planes A and C
	$x_{o,2}$
Figure D. 24:	Comparison of the secondary virtual origin D versus velocity ratio for the
	Primary jet under free conditions and with a base plate orientated at 60 degrees to
	the flow through planes A and C
Figure D. 25:	Comparison of the secondary decay constant K_2 versus the inverse velocity ratio
	for the secondary jet under free conditions and with a base plate orientated at 60
	degrees to the flow (WP) through planes A and B

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Figure D. 26:	Comparison of the secondary virtual origin	$x_{o,2}/D$	versus t	he inverse	velocity
	ratio for the secondary jet under free condition	ns with	a base p	late orientat	ted at 60
	degrees to the flow through planes A and B				

Nomenclature

Abbreviations and Constants

Aspect ratio	AR
Mean square error	MSE
Mean square regression	MSR
Signal to noise ratio	SNR
Sum square error	SSE
Regression sum of squares	SSR
Total sum of squares	SST

Roman Symbols

а	Regression coefficient
b	Regression coefficient
С	Regression coefficient
d	Regression coefficient
е	Regression coefficient
A	Jet Area
A_{ij}	Laser fluorescent response minus background
B_{ij}	Background image matrix
b_v	Velocity half-width
C	Concentration
C_{ref}	Reference concentration
$C_{1}, C_{2}C_{n}$	Proportionality constants
C_E	Entrainment Coefficient
D	Equivalent Diameter
D_e	Equivalent momentum diameter
D_f	Molecular diffusivity
d_i	Studentized residuals
d_p	Particle diameter
$\overline{F_o}$	F-Test value
H	Nozzle Height
I_{ii}	Laser distribution matrix
$\overset{{}_\circ}{J}$	Momentum Flux
k	Turbulent kinetic energy
Κ	Number of images
K_{l}	Centreline decay constant
K_2	Jet spread proportionality constant
L	Characteristic flow length
l_o	Integral scale
т	Mass flow rate
M_{ij}	Correction matrix

n	Empirical constants
Р	Pressure
P_{ij}	Raw measured fluorescent signal
\check{Q}	Volumetric flow rate
r	Radial coordinate
R	Accumulated background signal
<i>r</i> _{1/2}	Concentration half width
R^2	Coefficient of determination
R_i	Model response
S	Spacing between Jets
S_i	Sensitivity of Model response
Т	Temperature
t	Time
и	Velocity
u_s	Slip velocity between fluid and Particle
W	Nozzle Width
x	Jet axial direction
X	Averaged column of the laser fluorescent response minus background matrix
X_c	Axis switching cross over point
$x_{o, l}$	First order virtual origin
$x_{o,2}$	Second order virtual origin
У	Jet radial direction (major axis)
Ζ	Jet radial direction (minor axis)
\mathcal{Y}_{O}	Regression coefficient
Z_O	Regression coefficient

Greek Symbols

α	Regression Coefficient
β	Regression Coefficient
γ	Regression Coefficient
δ	Regression Coefficient
ε	Rate of turbulent dissipation
ϕ	Quantum yield
γ	Secondary to primary jet momentum flux ratio
arphi	Secondary to primary jet mass flow ratio
К	Secondary to primary jet momentum ratio
Ķ	Modified secondary to primary jet momentum ratio
λ	Secondary to primary jet velocity ratio
λ'	Modified secondary to primary jet velocity ratio
λ_B	Batchelor Scale
λ_T	Taylor microscale
μ	Dynamic Viscosity
ν	Dimensionless radial coordinate
$ ho_{f}$	Fluid density
$ ho_p$	Particle density
$ ho_s$	Source density

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σ	Standard Deviation
$ au_B$	Temporal Batchelor Scale
$ au_{f}$	Fluid response time
$ au_p$	Particle response time
V	Kinematic Viscosity
arOmega	Level of uncertainty
ξ	Mixture fraction

Non Dimensional Parameters

Ре	Peclet number = $\frac{\overline{u}D}{D_f}$
Re, Re _f	Fluid Reynolds number = $\frac{\overline{u}D}{v}$
Re_{bv}	Local velocity based half width Reynolds number = $\frac{\overline{uD}}{v}$
Re_p	Particle Reynolds Number = $\frac{\overline{u_s}d_p}{v}$
Sc	Schmidt number = $\frac{v}{D_f}$
St	Stokes number = $\frac{\overline{u}(d_p)^2}{18\nu L}$
Stl	Strouhal Number = $\frac{D}{tu}$

Subscripts/Superscripts

Denotes quantity from primary jet	1
Denotes quantity from secondary jet	2
Denotes quantity from surrounding fluid	3
Denotes fluctuating quantity	'
Denotes time-averaged quantity	-
Denotes range of confidence for F-test	α
Bulk mixture quantity	В
Denotes centreline quantity	С
Matrix column	i
Matrix row	j
Matrix number in a 3-D matrix	k
Degrees of freedom	т
Degrees of freedom	n
Denotes quantity at jet source	0
Denotes measured quantity with laser off	off
Denotes measured quantity with laser on	on
Primary bulk mixture quantity	PB
Random mean square quantity	rms

Secondary bulk mixture quantity Denotes total combined bulk mixture quantity

SB TB